



Energy Efficient GO-PEEK Hybrid Membrane Process for Post-combustion CO₂ Capture

DOE Contract No. DE-FE0026383

Shiguang Li

Gas Technology Institute (GTI)

Miao Yu

University of South Carolina (USC), and Rensselaer Polytechnic Institute (RPI)

Yong Ding

Air Liquide Advanced Separations (ALaS)



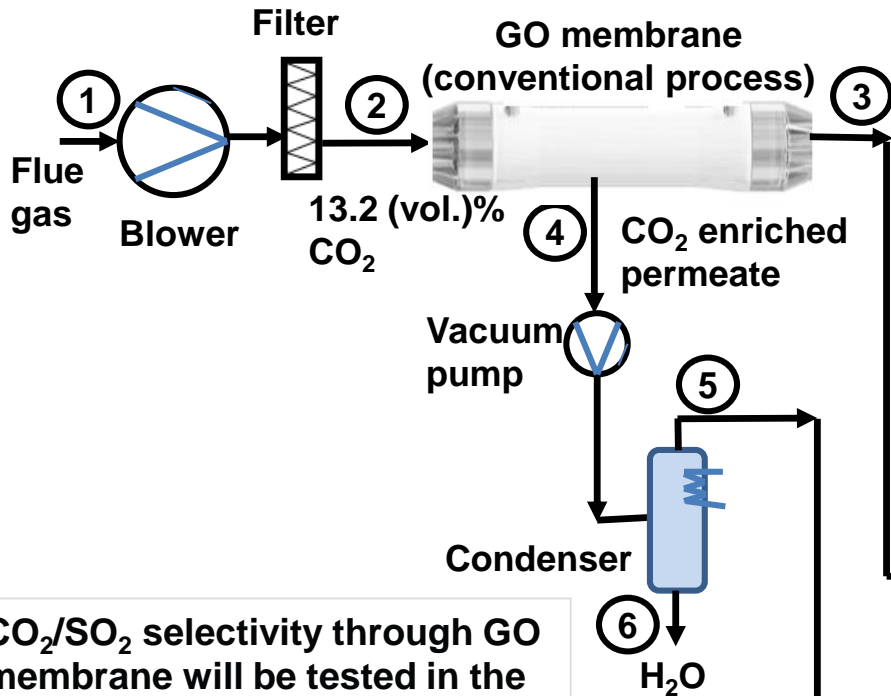
CO₂ Capture Technology Project Review Meeting

August 21 - 25, 2017, Pittsburgh, PA

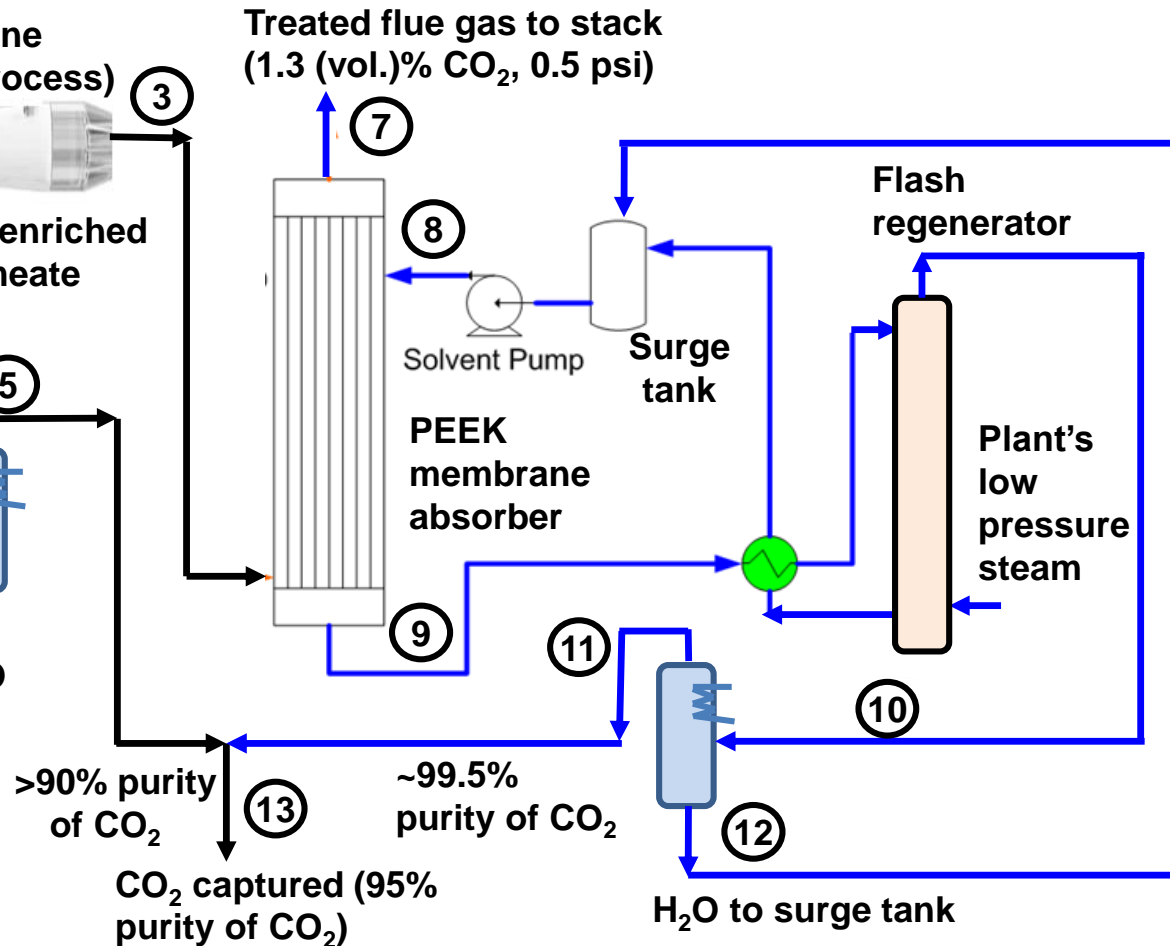


Process description

GO for bulk/partial CO₂ removal



PEEK HFMC to further capture CO₂








CO₂/SO₂ selectivity through GO membrane will be tested in the current program:

- **Case 1:** SO₂ permeates through the membrane, a caustic scrubber is needed before the GO membrane
- **Case 2:** SO₂ stays in the retentate, scrubber unneeded; HFMC can handle 150 ppmv SO₂ (DE-FE-0004787)

GO = graphene oxide

GO-PEEK project overview

- **Performance period**: Oct. 1, 2015 – Sep. 30, 2018
- **Funding**: \$1,999,995 from DOE; \$500,000 cost share
- **Objectives**: Develop a hybrid membrane process combining a graphene oxide (GO) gas separation membrane configuration unit and a PEEK hollow fiber membrane contactor (HFMC) unit to capture $\geq 90\%$ of the CO_2 from flue gases with 95% CO_2 purity at a cost of electricity 30% less than the baseline CO_2 capture approach
- **Team**:

Member	Roles
	<ul style="list-style-type: none"> • Project management and planning • Quality control and CO_2 capture performance tests
 	<ul style="list-style-type: none"> • GO membrane development
 ALaS	<ul style="list-style-type: none"> • PEEK membrane development
	<ul style="list-style-type: none"> ■ High-level technical & economic feasibility study

GO membrane technology based on our pioneering work published in *Science* (2013, 342 (6154) 95)

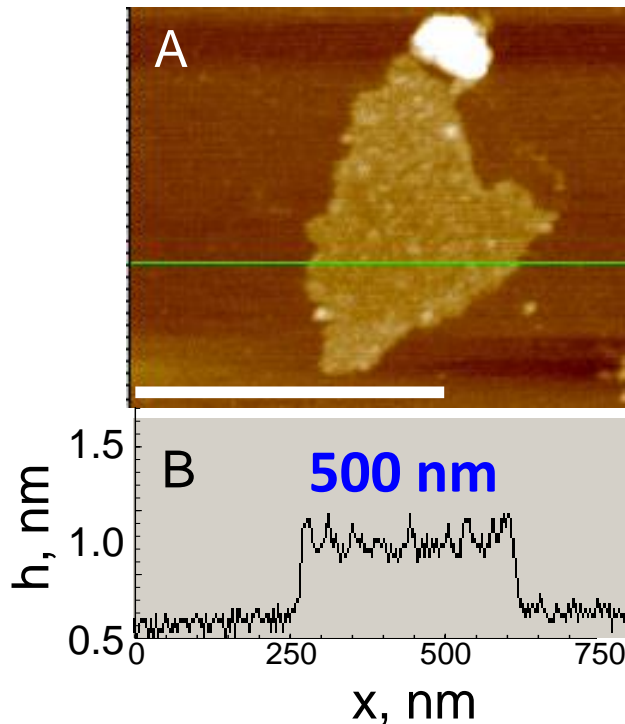


Ultrathin, Molecular-Sieving Graphene Oxide Membranes for Selective Hydrogen Separation

Hang Li *et al.*

Science **342**, 95 (2013);

DOI: 10.1126/science.1236686

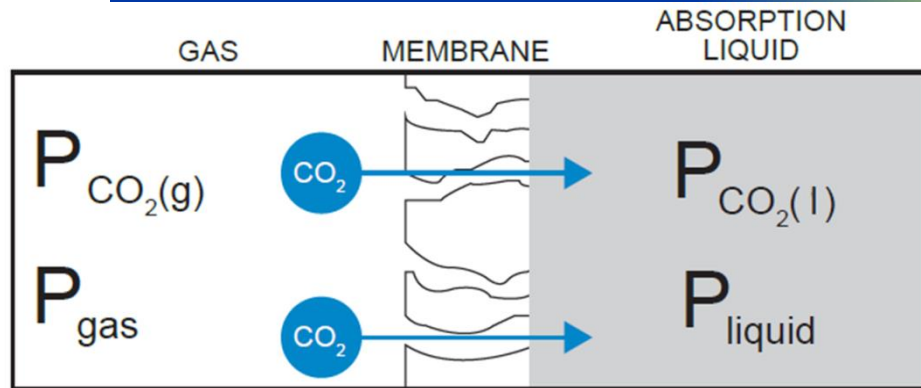


■ Contribution of the paper:

- Structural defects on GO flakes can be controlled as transport pathway for selective gas separations

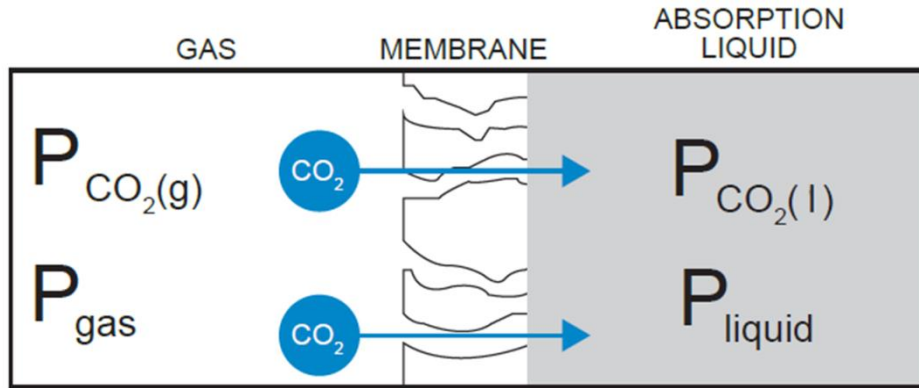
Single-layered GO flake
prepared as thin as 1 nm

Singular PEEK HFMC technology currently at pilot scale development stage (DE-FE0012829)



Membrane contactor: high surface area device that facilitates mass transfer

Singular PEEK HFMC technology currently at pilot scale development stage (DE-FE0012829)

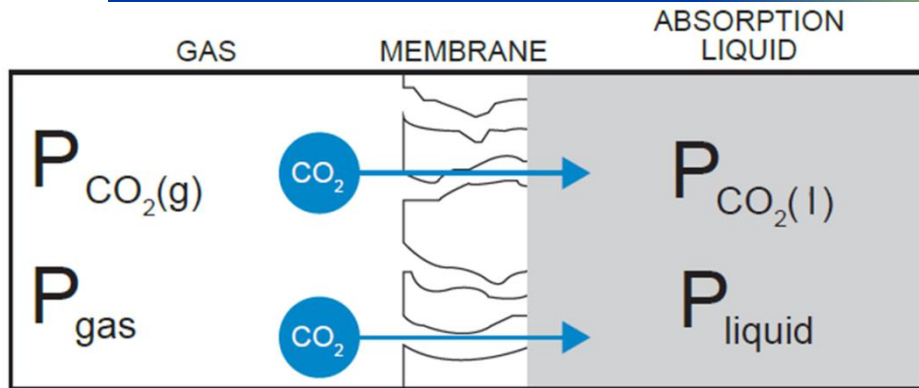


Membrane contactor: high surface area device that facilitates mass transfer



Commercial-sized modules

Singular PEEK HFMC technology currently at pilot scale development stage (DE-FE0012829)



Membrane contactor: high surface area device that facilitates mass transfer



Commercial-sized modules

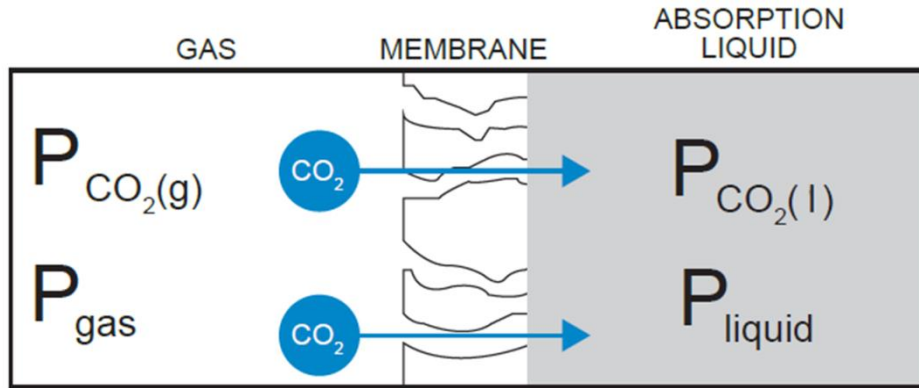


NCCC PSTU system
(0.5 MW_e)

GTI HFMC system
(0.5 MW_e)

Plant constructed and installed at NCCC

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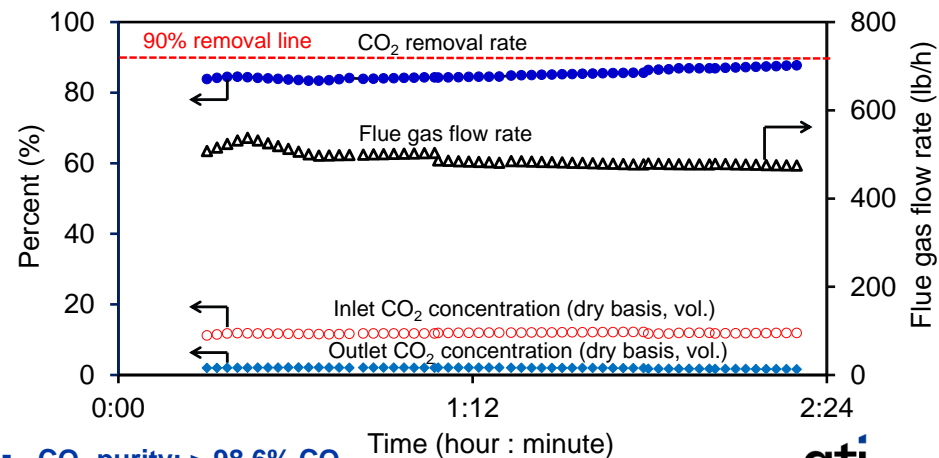
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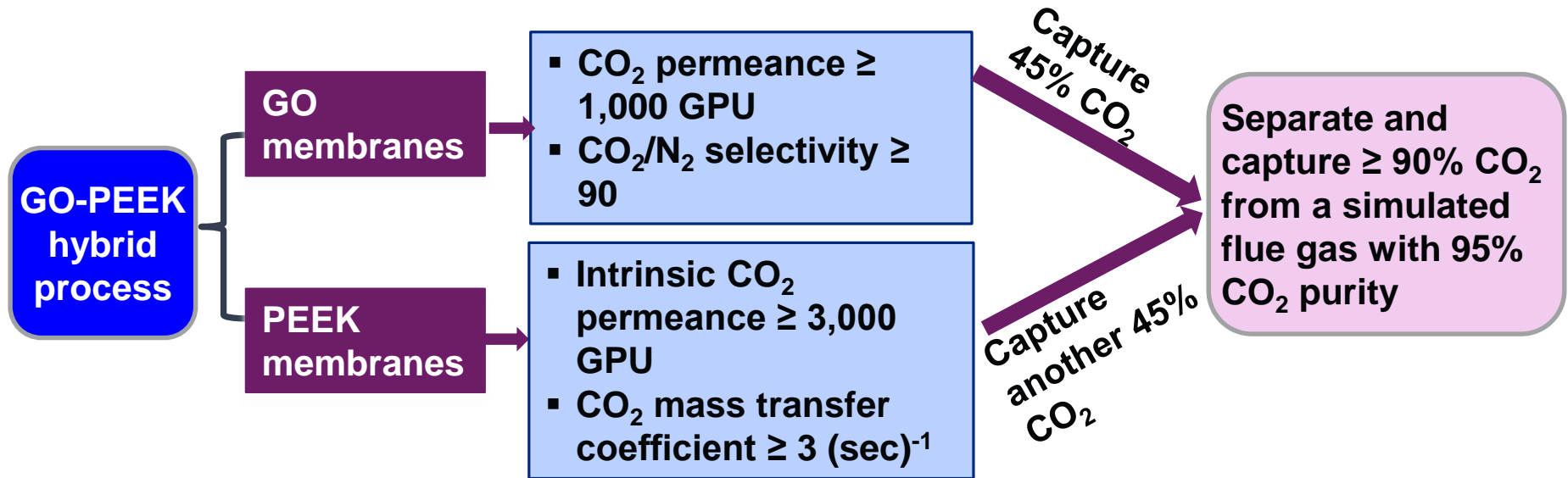
NCCC testing results indicate DOE's technical target can be achieved

CO₂ removal rate:

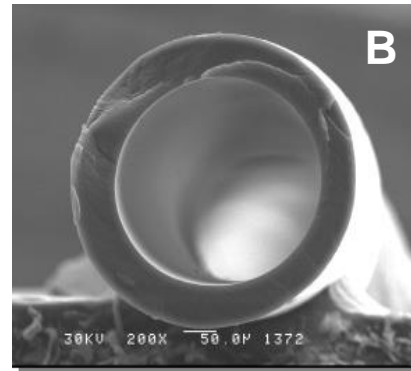
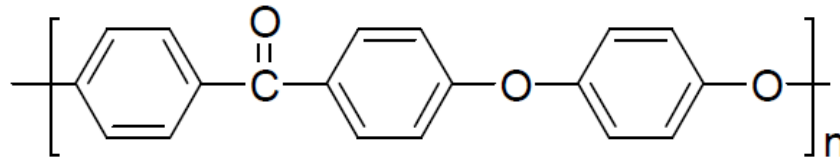


CO₂ purity: > 98.6% CO₂

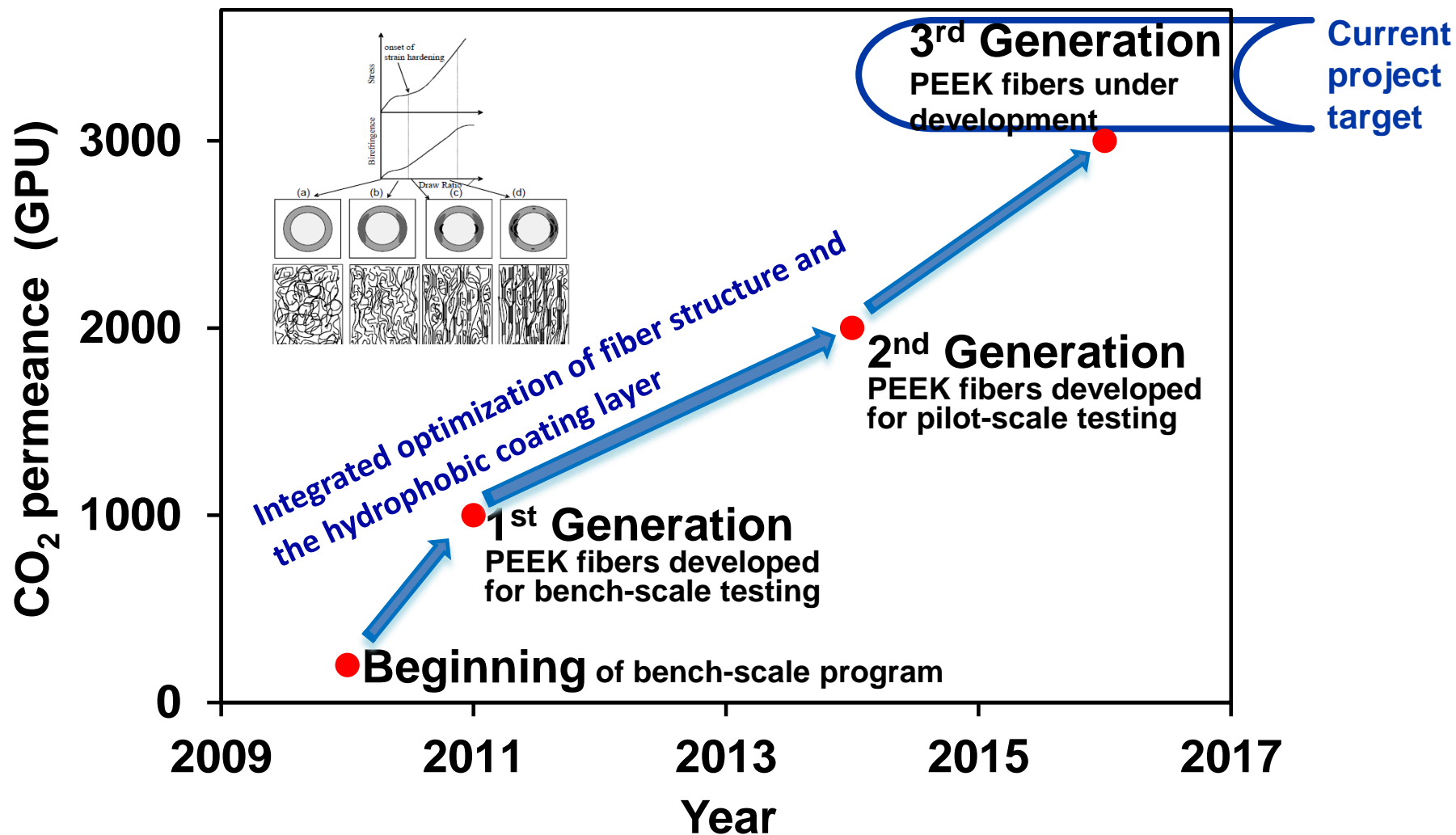
GO-PEEK technical goals



Progress on PEEK Membranes



Under the current program, we are developing PEEK fibers with intrinsic CO₂ permeance of 3,000 GPU



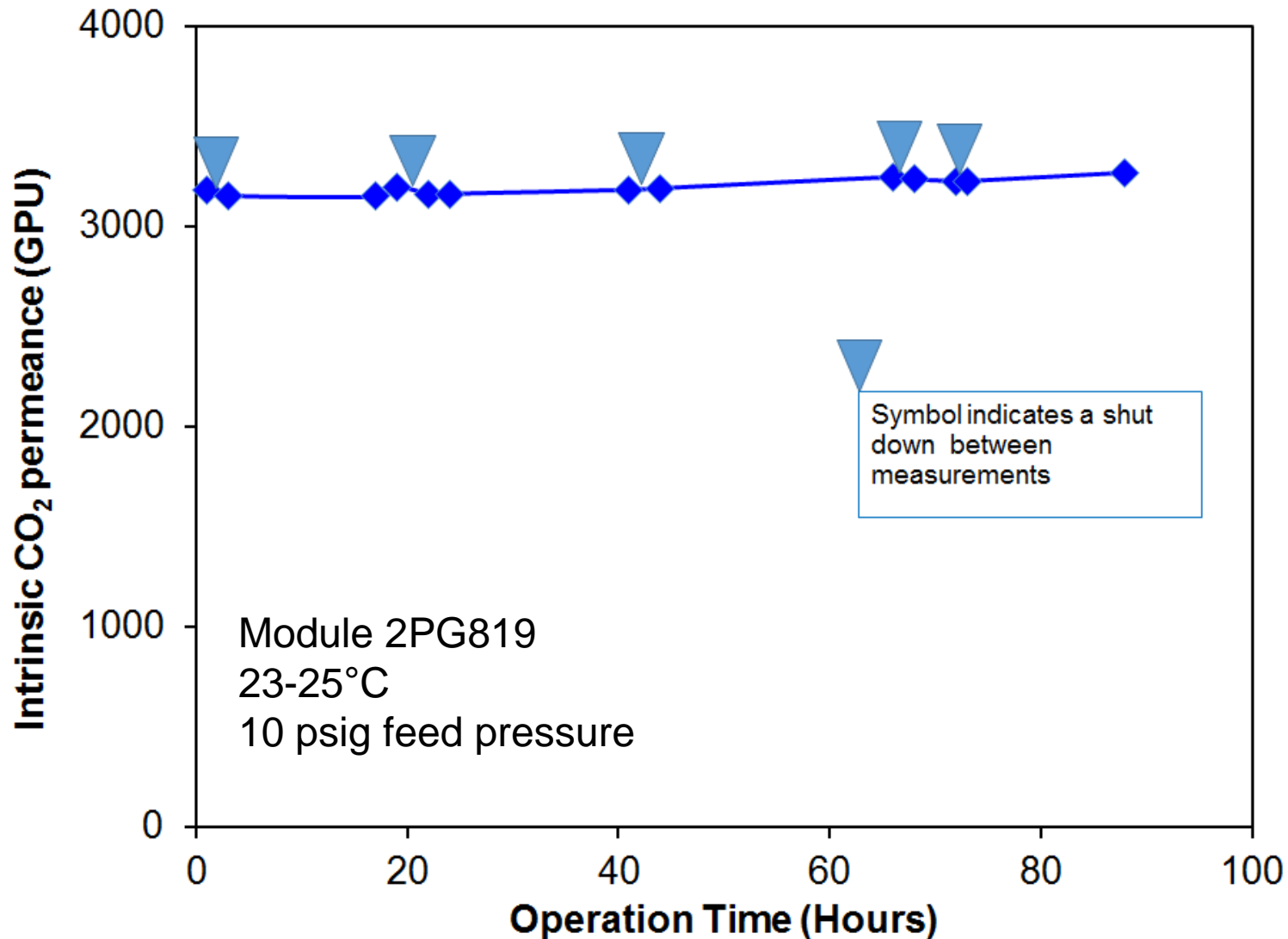
1 GPU = 1 x 10⁶ cm³ (STP)/cm² • s • cmHg

Eight types of fibers were investigated

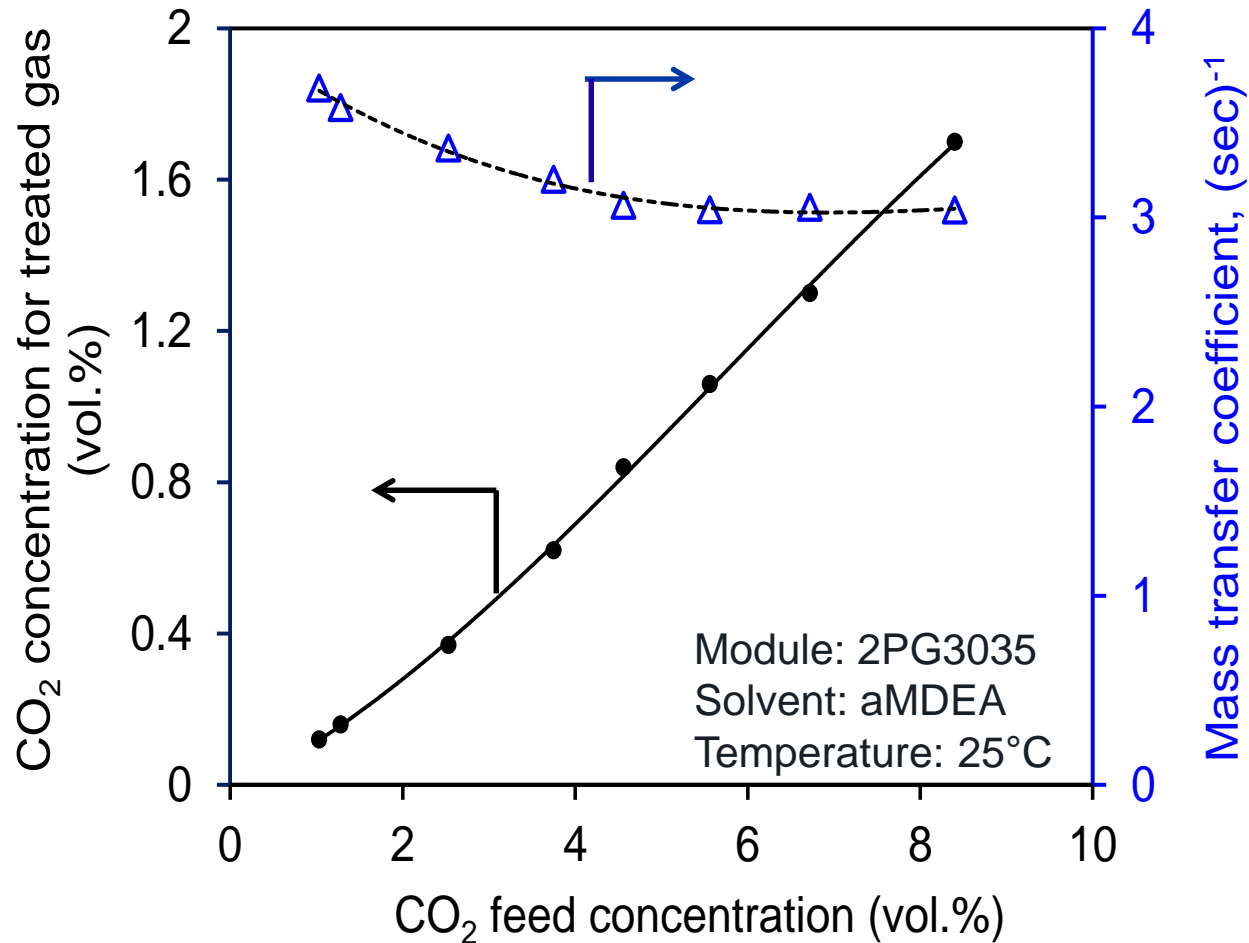
Sample No.	Fiber OD (Micron)	Fiber ID (Micron)	CO ₂ permeance* (GPU)
78-33-3A	582	350	2,300
78-33-3B	582	350	2,500
78-118-3A	569	358	2,300
78-118-3B	569	358	2,800
78-117-5A	569	353	3,400
78-117-5B	569	353	3,400
78-117-5C	569	353	3,700
78-117-5D	569	353	3,800

Temperature: 25°C, feed pressure: ~ 5 psig

2-inch module 2PG819 containing 78-117-5C fibers (CO₂ permeance of 3,700 GPU)

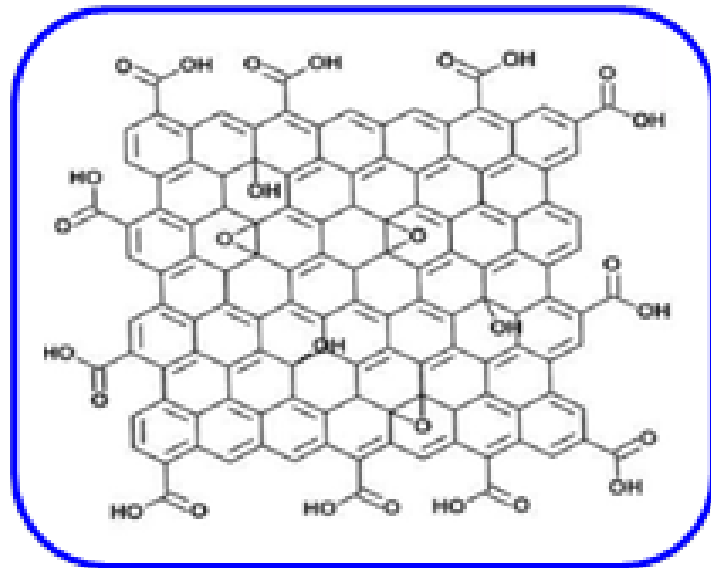


PEEK membrane module effective in capturing CO₂ from low CO₂-concentration feeds in membrane contactor



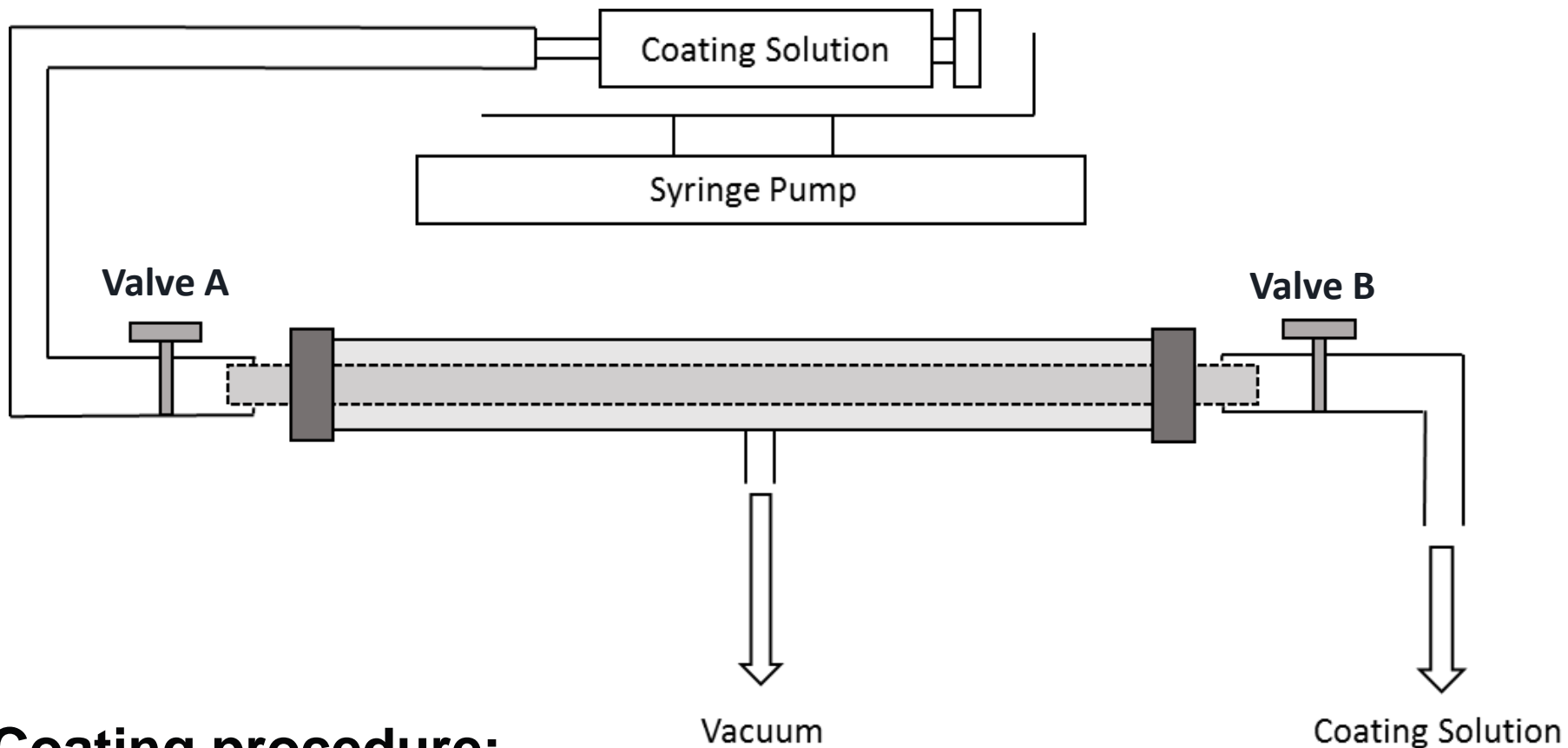
Goal of mass transfer coefficient > 3 (sec)⁻¹ achieved

Progress on GO Membranes



GO: single-atomic layered, oxidized graphene

Procedure developed for coating GO-based membrane on hollow fiber (HF) support

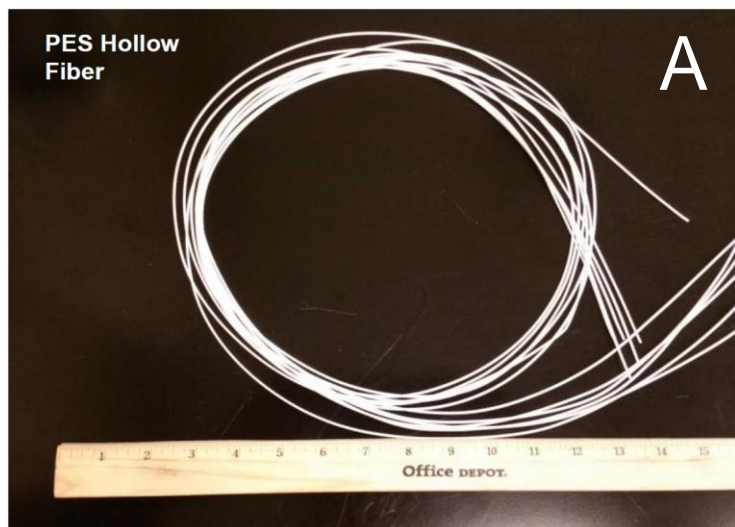


Coating procedure:

1. Valves A and B are open, GO dispersion flows continuously in hollow fiber
2. Vacuum filtration is conducted for a controlled time; and
3. Valves A and B are closed; coated fiber stays under vacuum for a controlled time

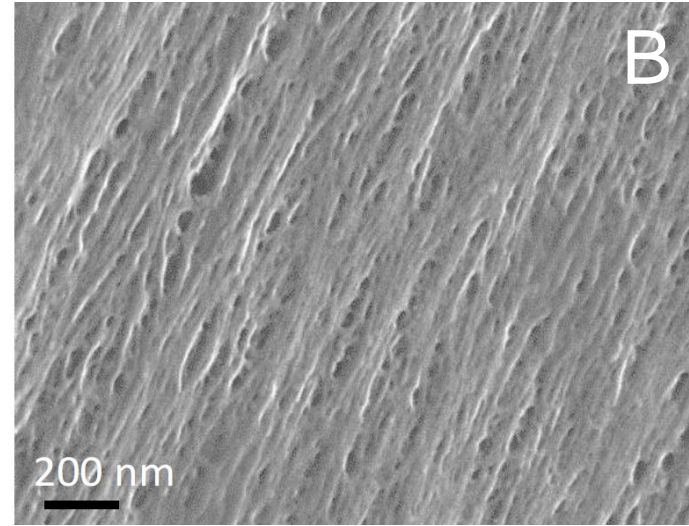
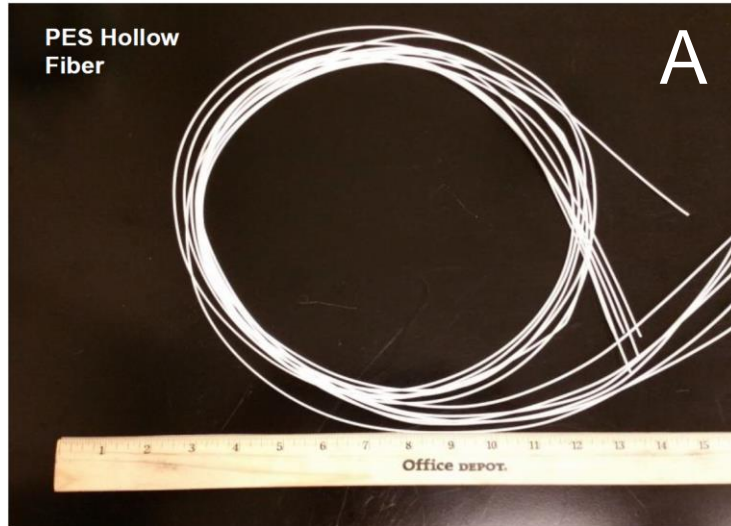
GO membrane (thickness: ~9 nm) supported on polyethersulfone (PES) hollow fiber

PES
fiber



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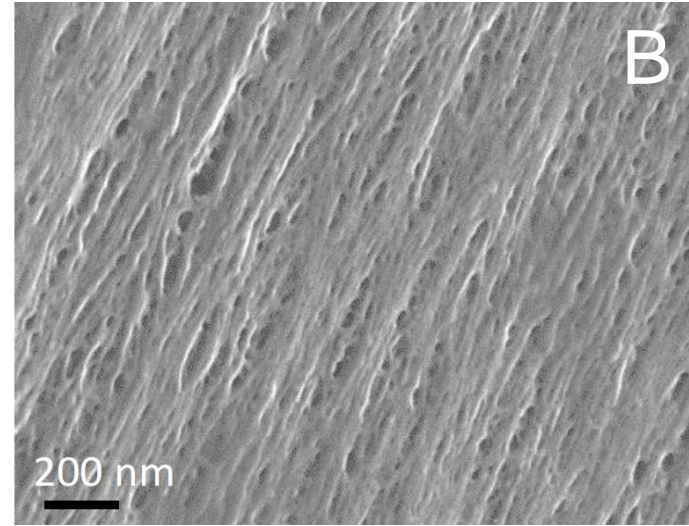
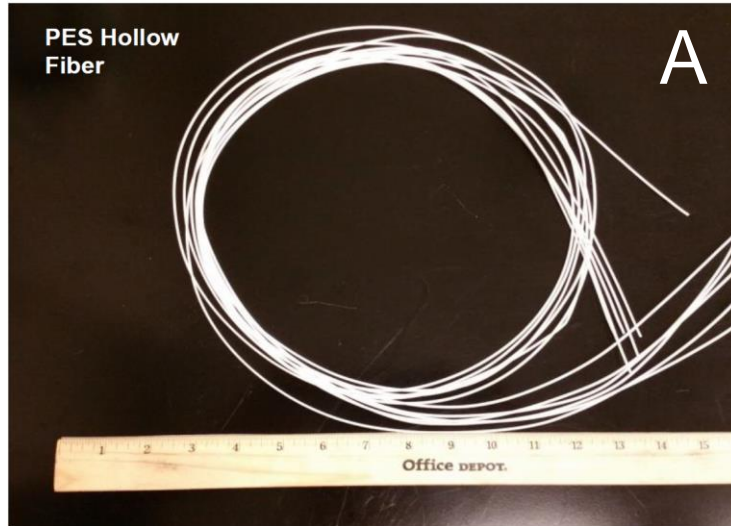
PES
fiber



Uncoated
fiber
surface

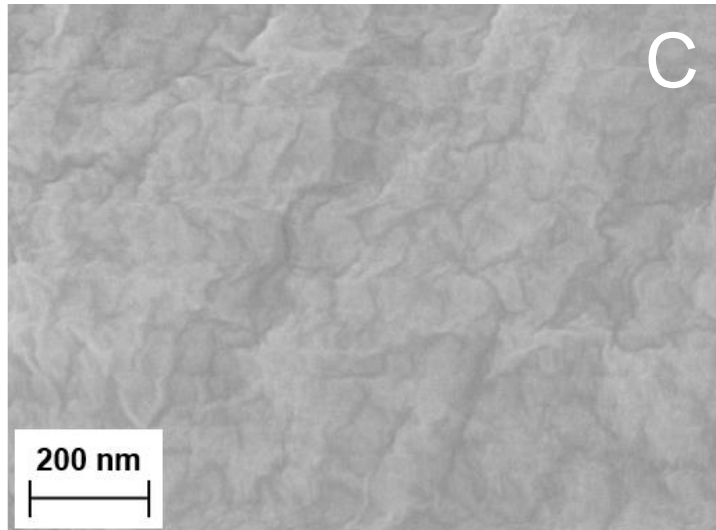
GO membrane (thickness: ~9 nm) supported on polyethersulfone (PES) hollow fiber

PES
fiber



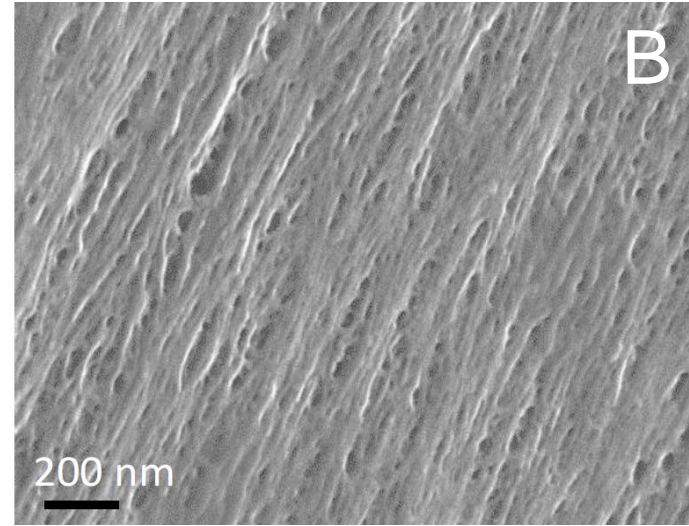
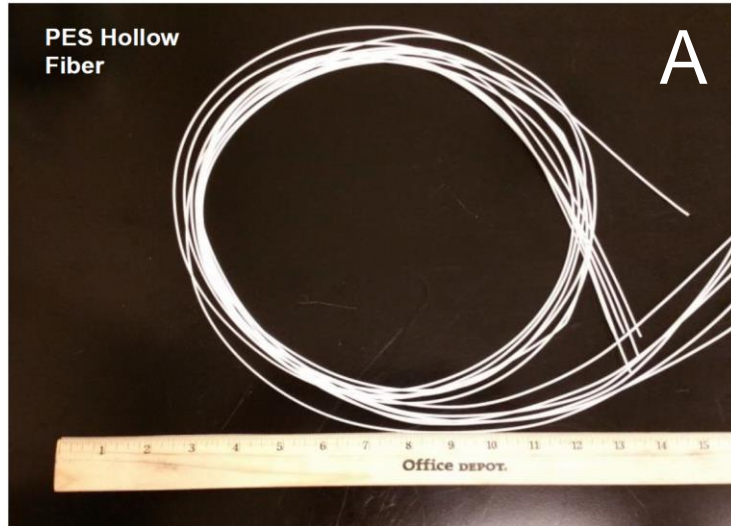
Uncoated
fiber
surface

Coated
fiber
surface



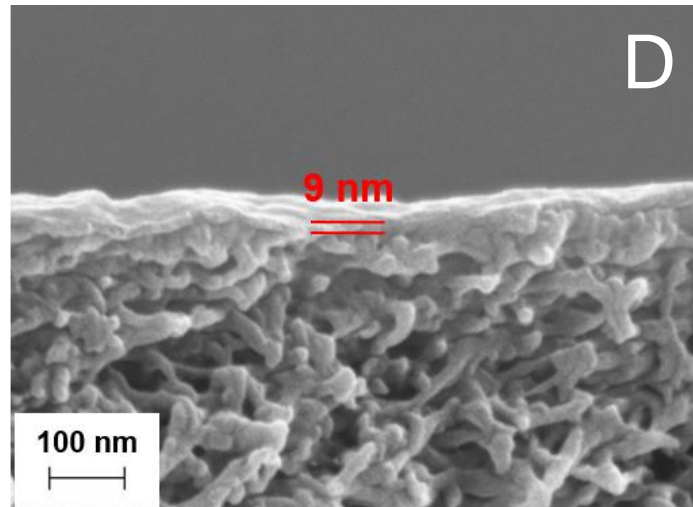
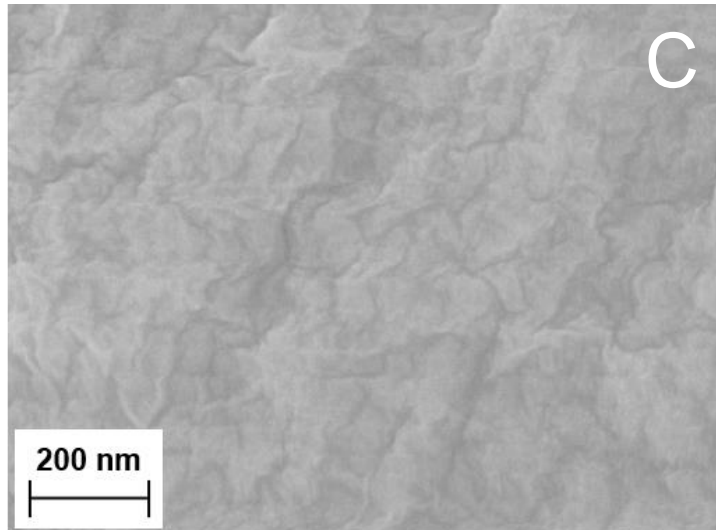
GO membrane (thickness: ~9 nm) supported on polyethersulfone (PES) hollow fiber

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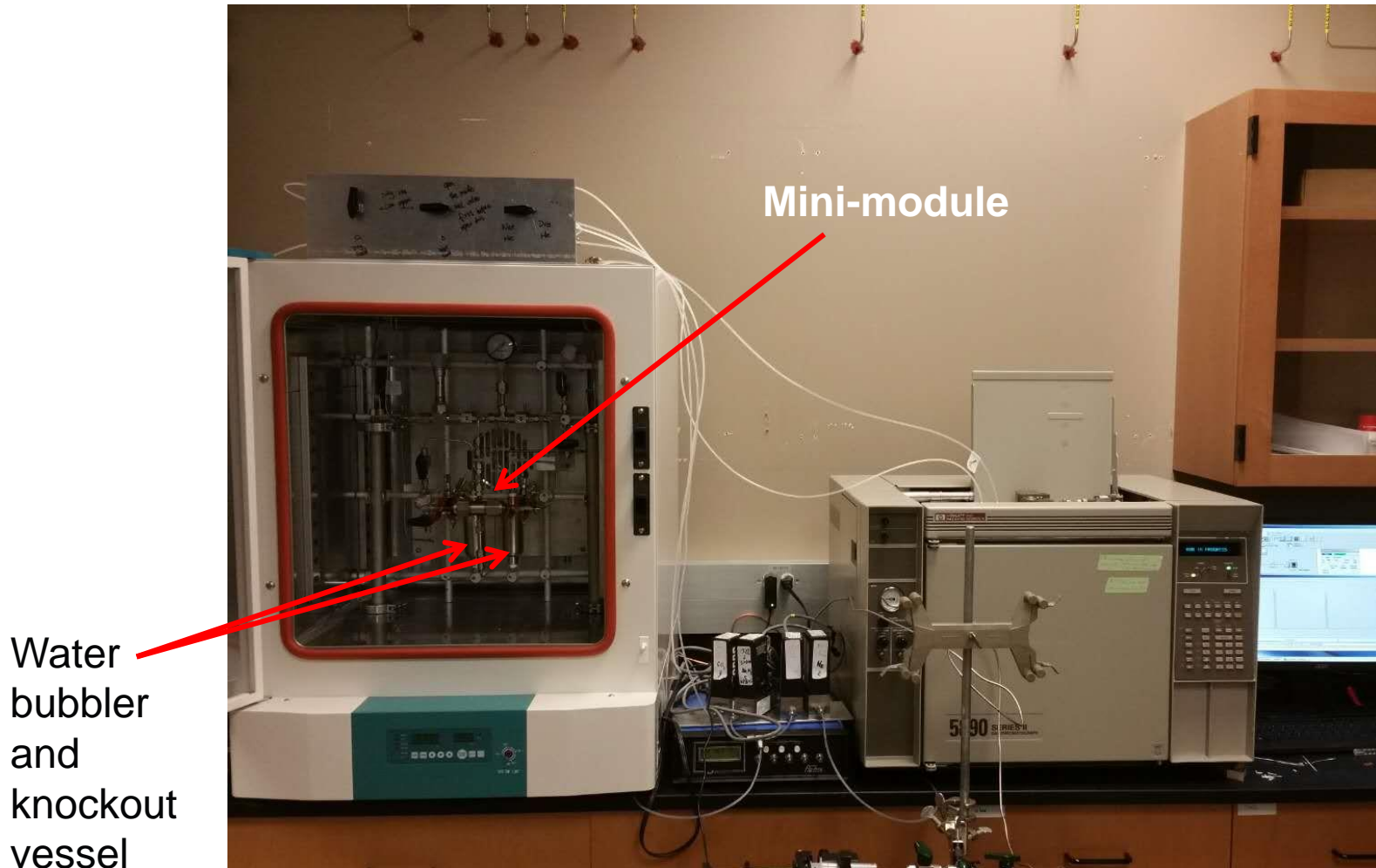
Coated
fiber
surface



Coated
fiber cross
section

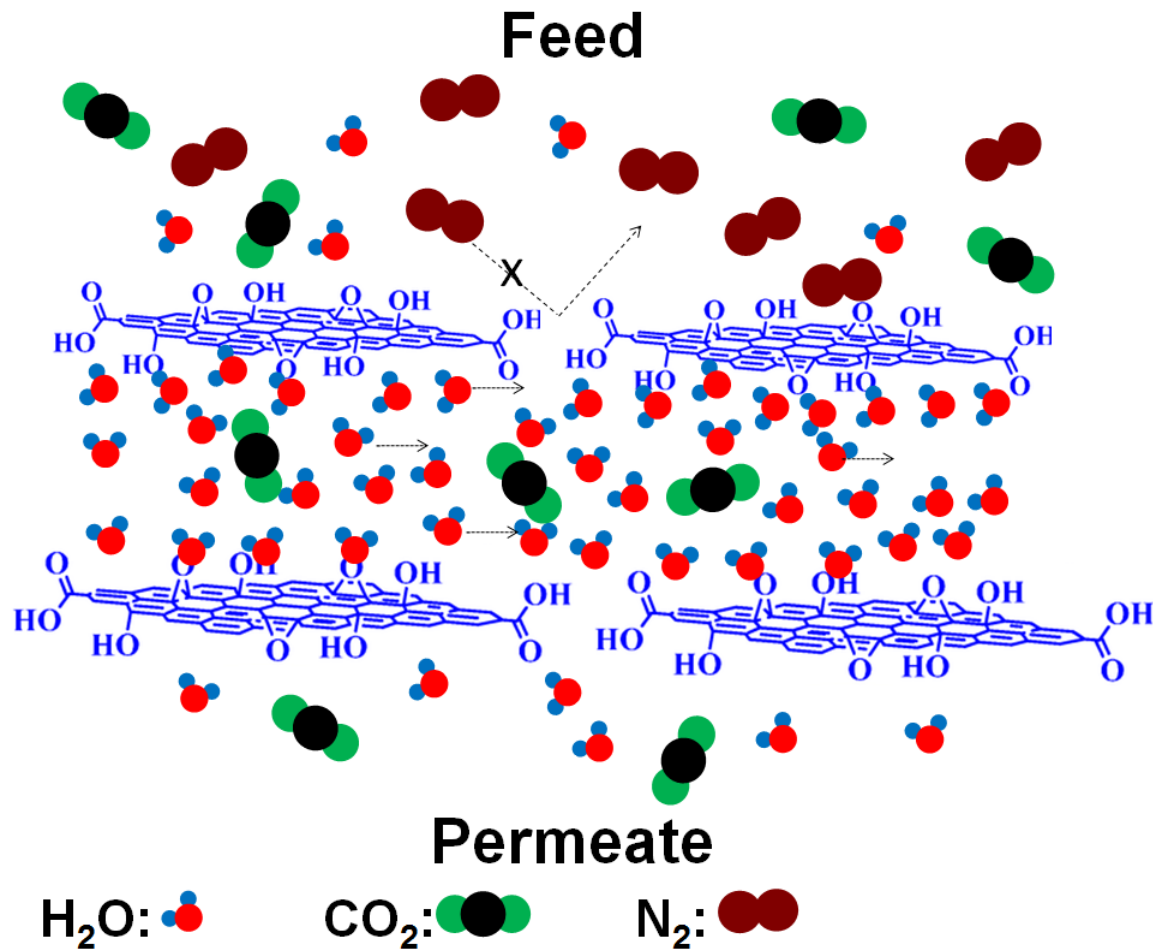
Coated fiber sealed in a mini-module for gas permeation testing

Permeation testing unit

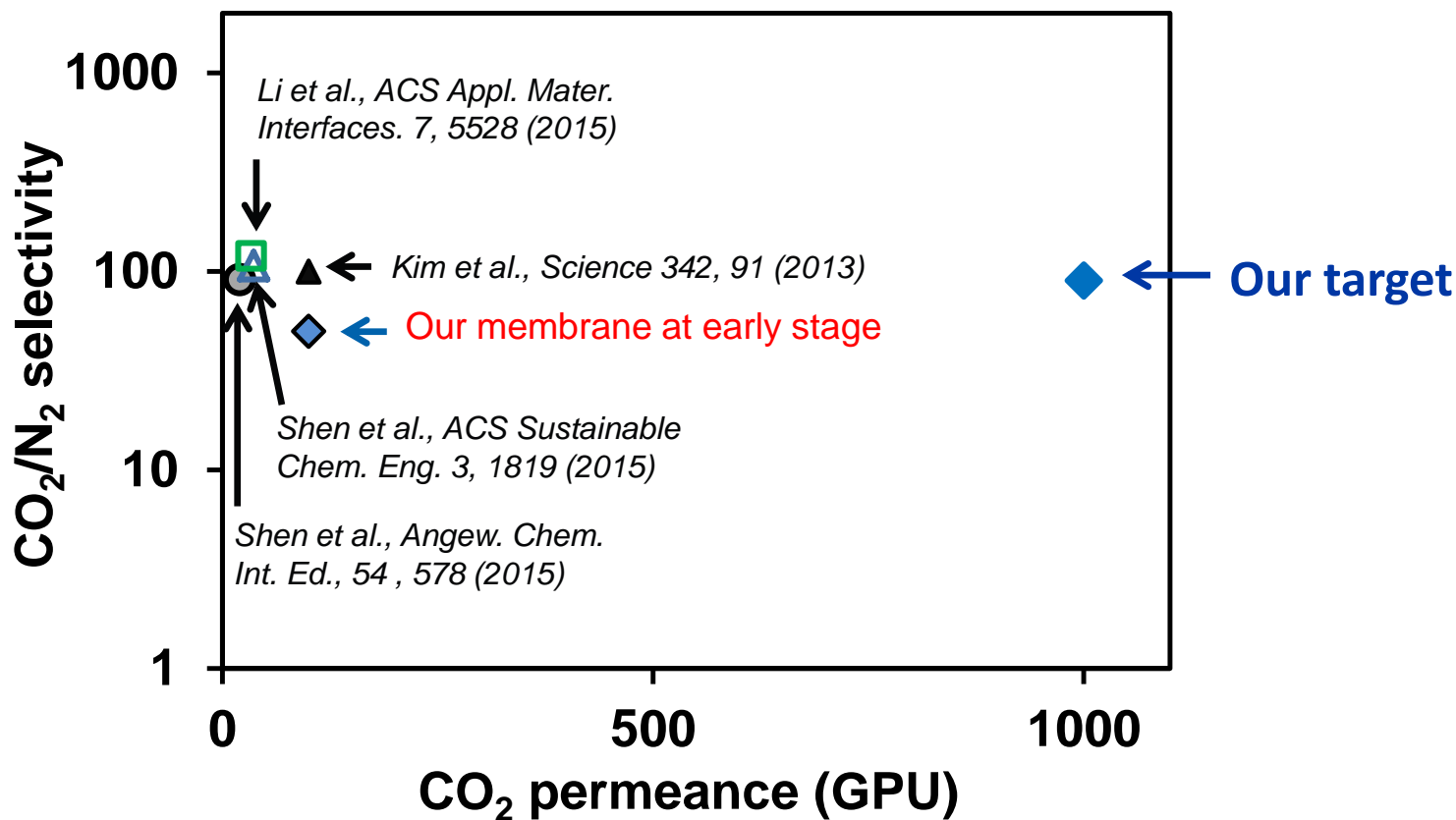


Initial GO membrane performance under simulated flue gas condition

- CO₂ permeance of 100 GPU and selectivity of 49 obtained for a humidified 15%/85% CO₂/N₂ mixture

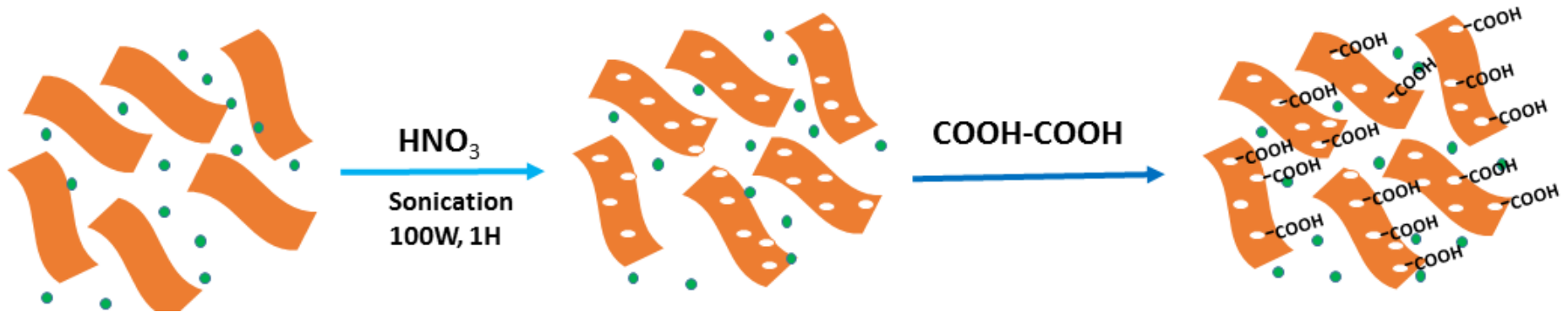


Challenge: GO membrane performance needs significant improvement



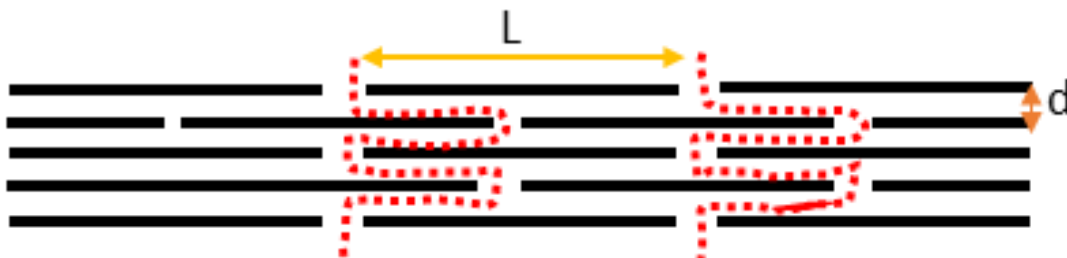
Approaches to improve CO₂ permeance

- Create more structural defects on GO flake by HNO₃ etching

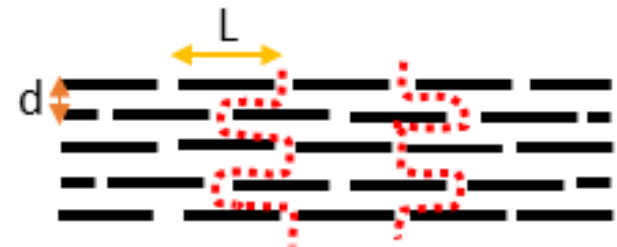


- Reduce GO flake lateral size by ultra-sonication

W/O ultra-sonication

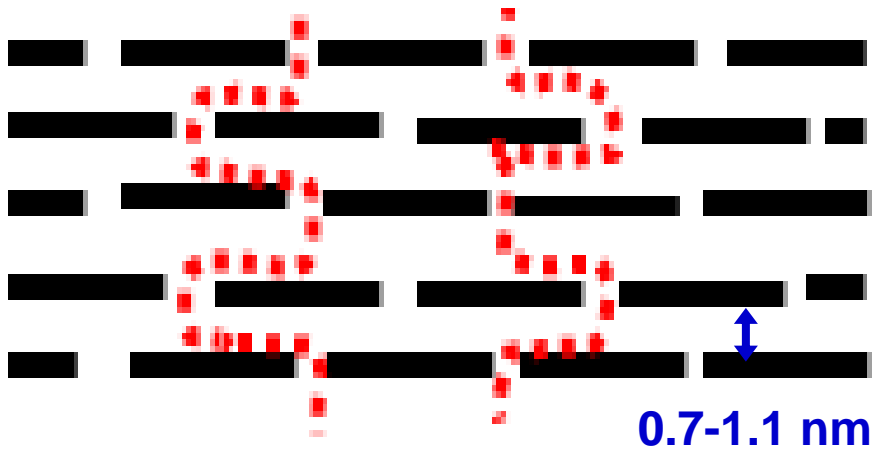


W/ ultra-sonication



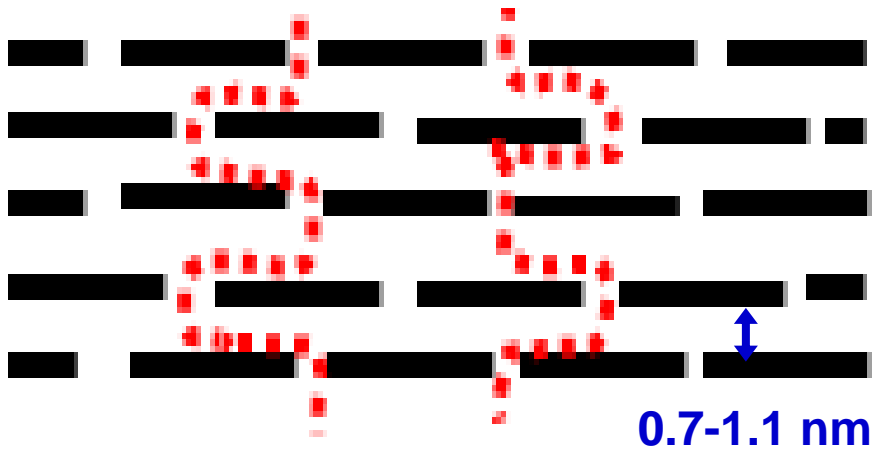
Approach to improve CO₂/N₂ selectivity: fill the space between GO layers with CO₂-philic agent

- CO₂-philic agent enables facilitated transport mechanism to separate CO₂ from N₂

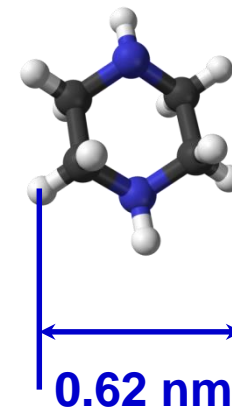


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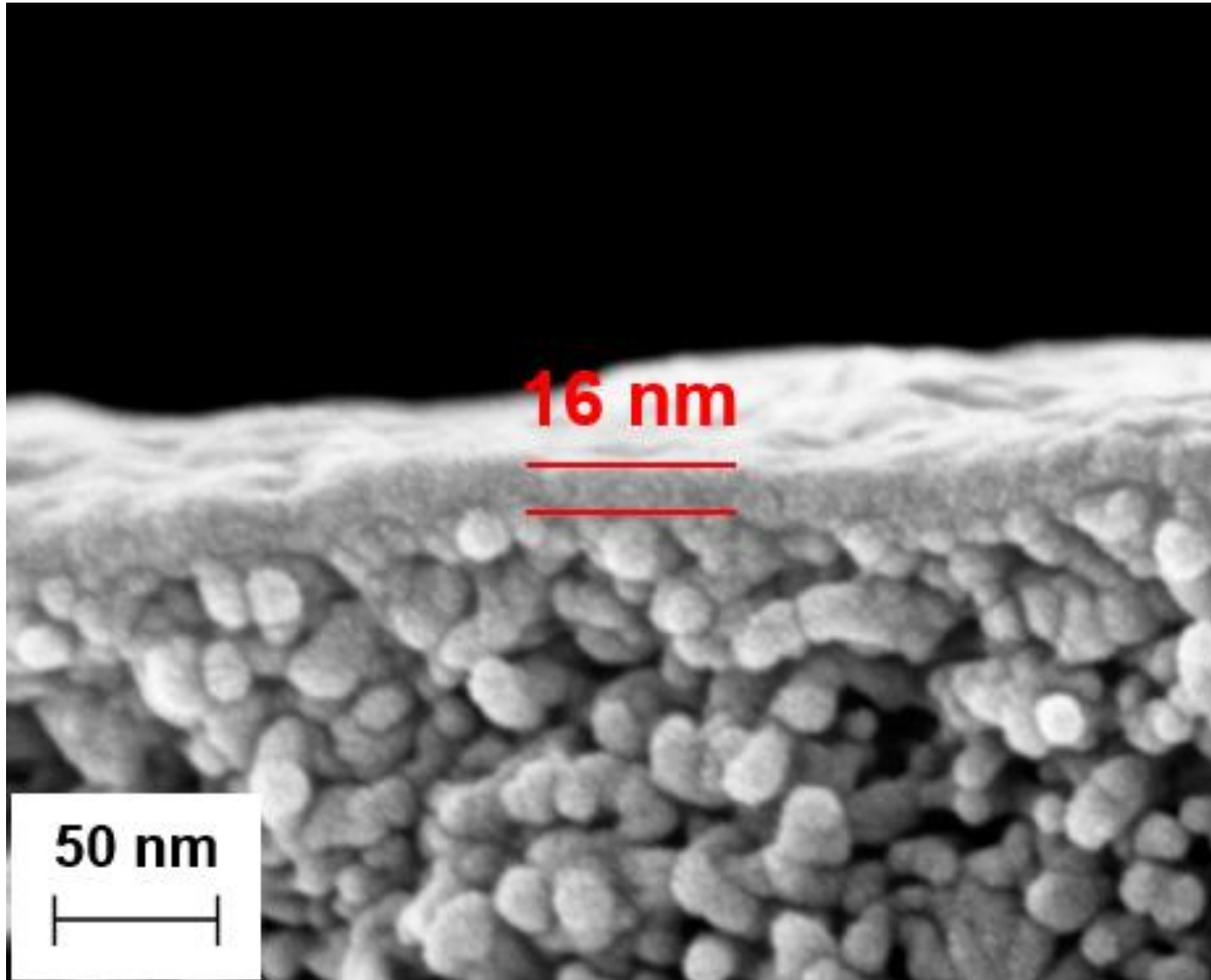
- CO₂-philic agent enables facilitated transport mechanism to separate CO₂ from N₂



CO₂-philic agent example:
piperazine (PZ)

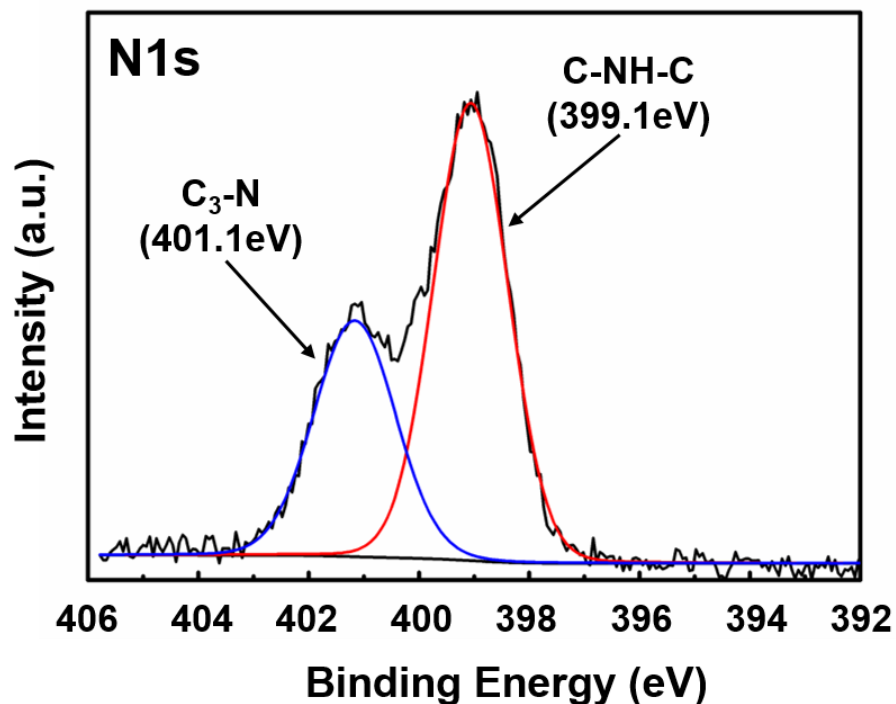


Cross-sectional SEM of the PZ filled GO membrane

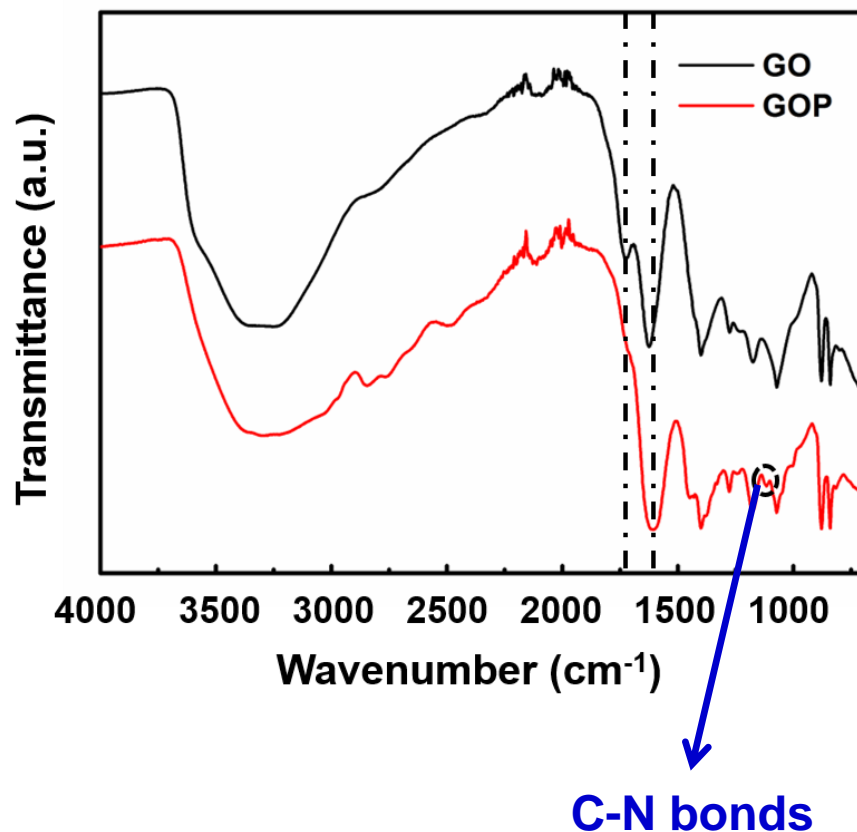


XPS and FTIR analysis confirmed the crosslinking of PZ with GO sheets

XPS



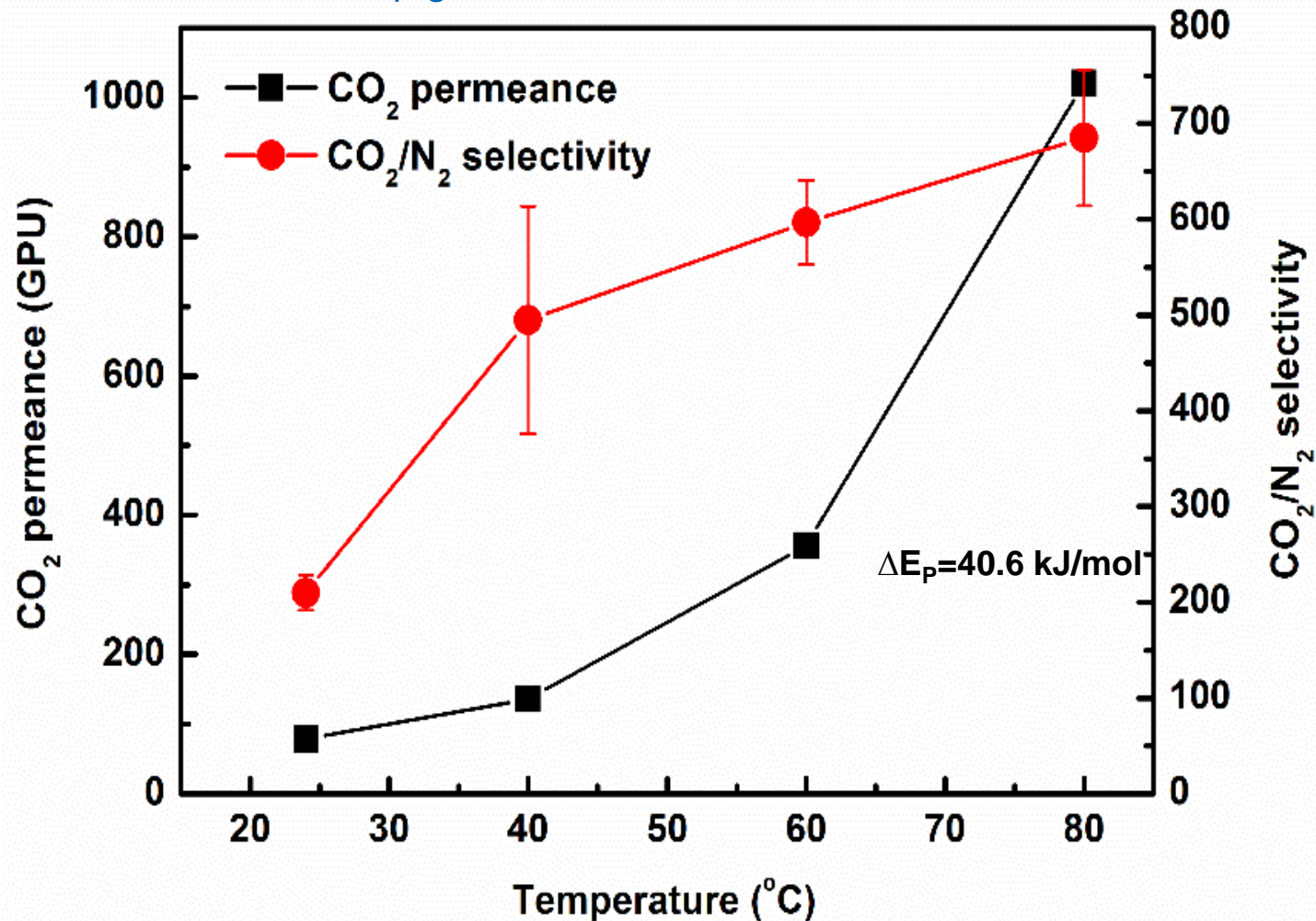
FTIR



GO-based membranes separation performance

Feed: 15% CO₂/85%N₂ with saturated water vapor

Permeate: with sweep gas

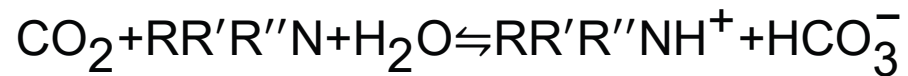


Facilitated transport mechanism

-

0.7-1.1 nm

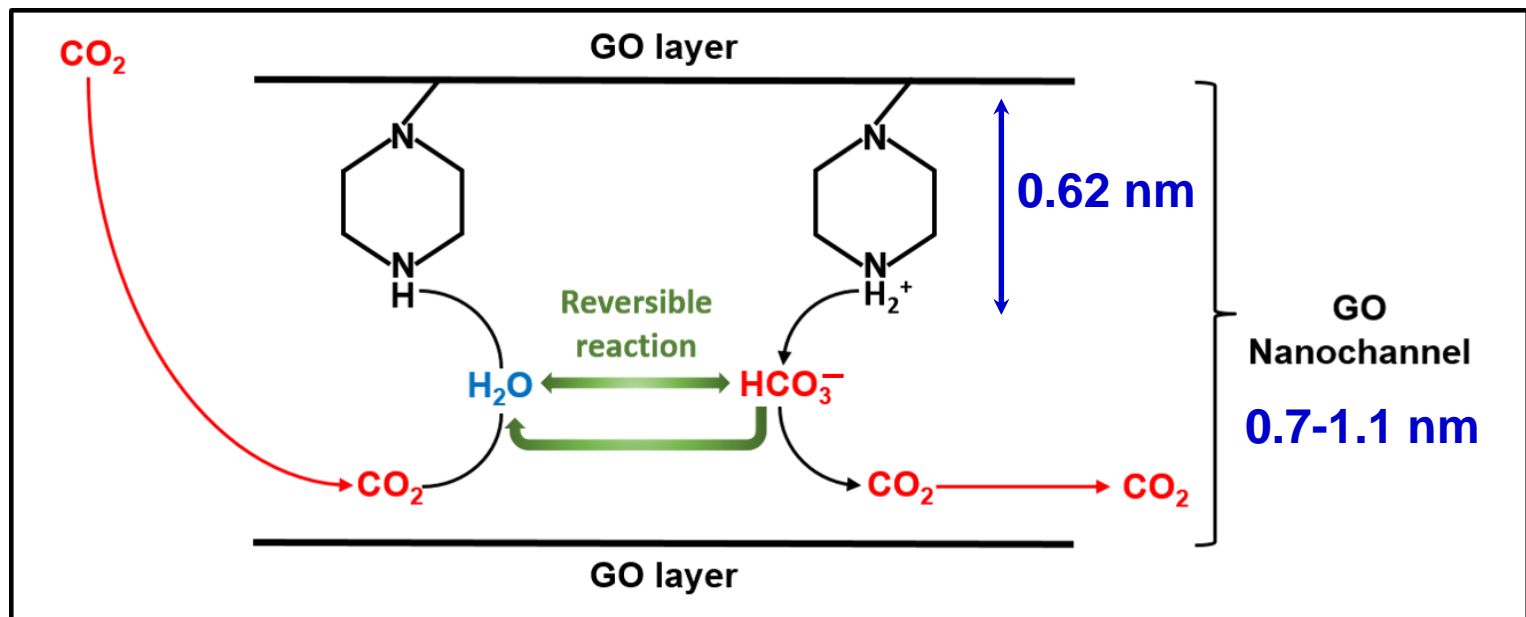
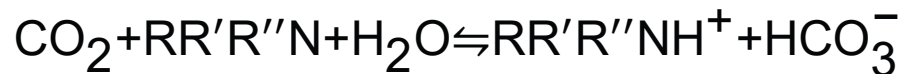
Facilitated transport mechanism



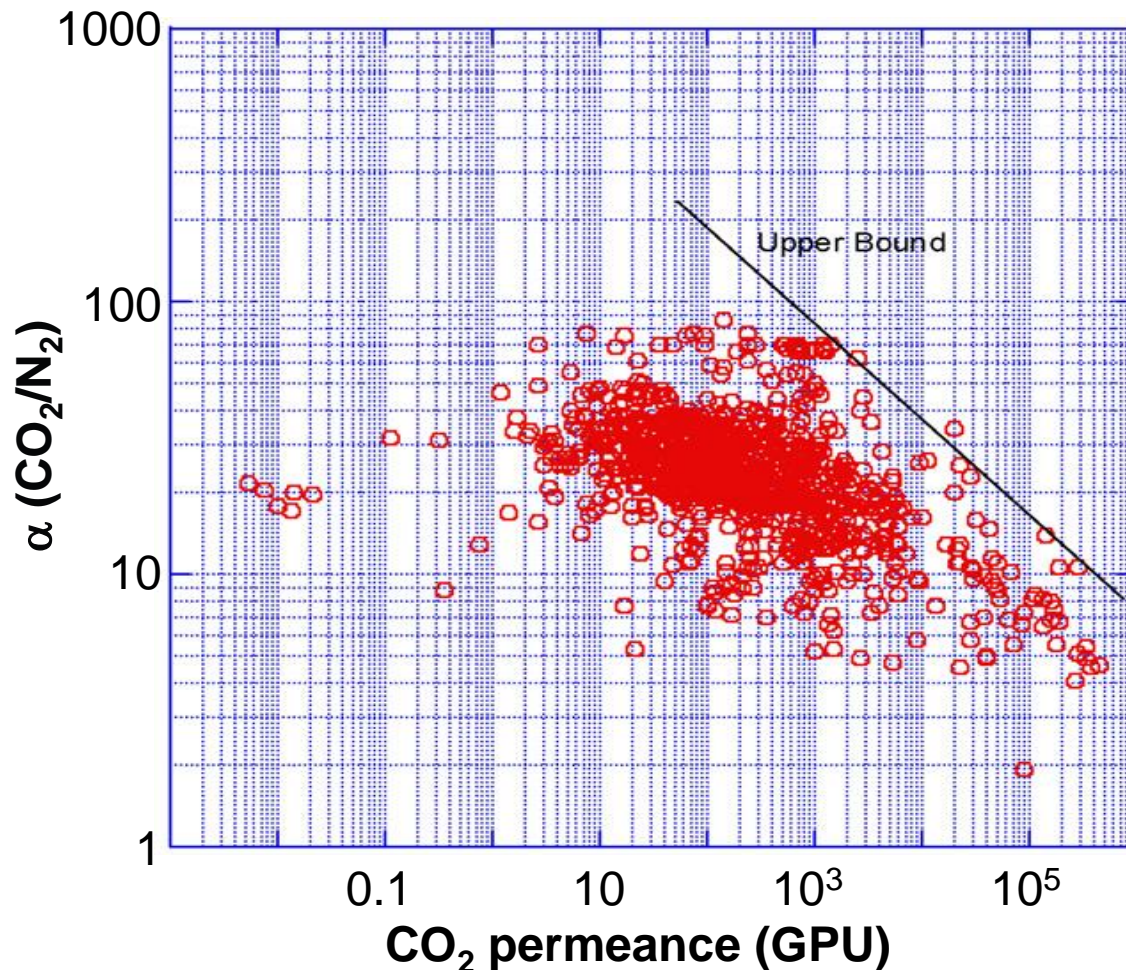
-

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Facilitated transport mechanism



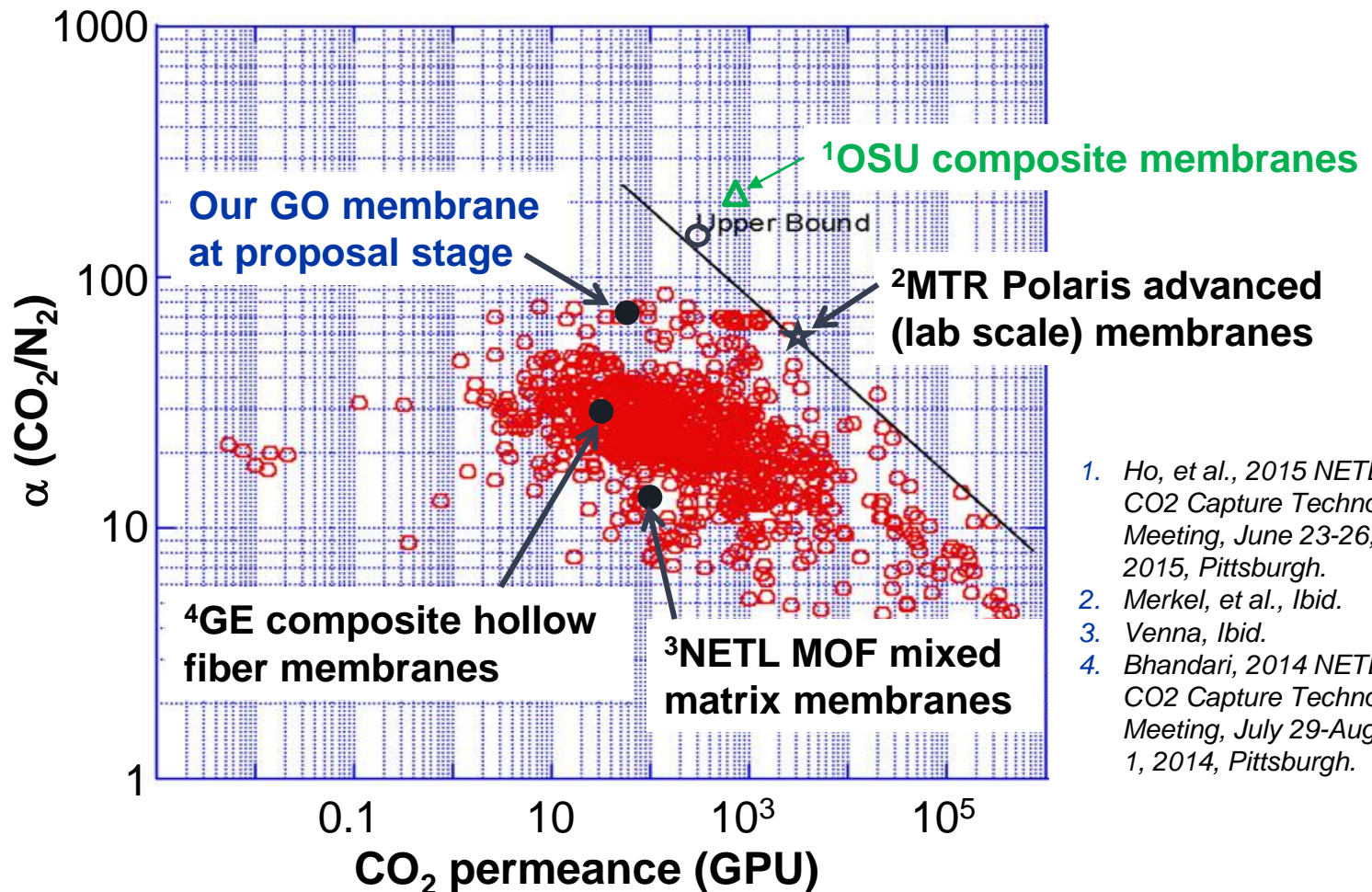
Comparison to other CO₂/N₂ separation membranes



Robeson, J. *Membrane Sci.* **2008**, Vol. 320, p390

Note: Polymer data points (red): 100 nm membrane thickness assumed

Comparison to other CO₂/N₂ separation membranes

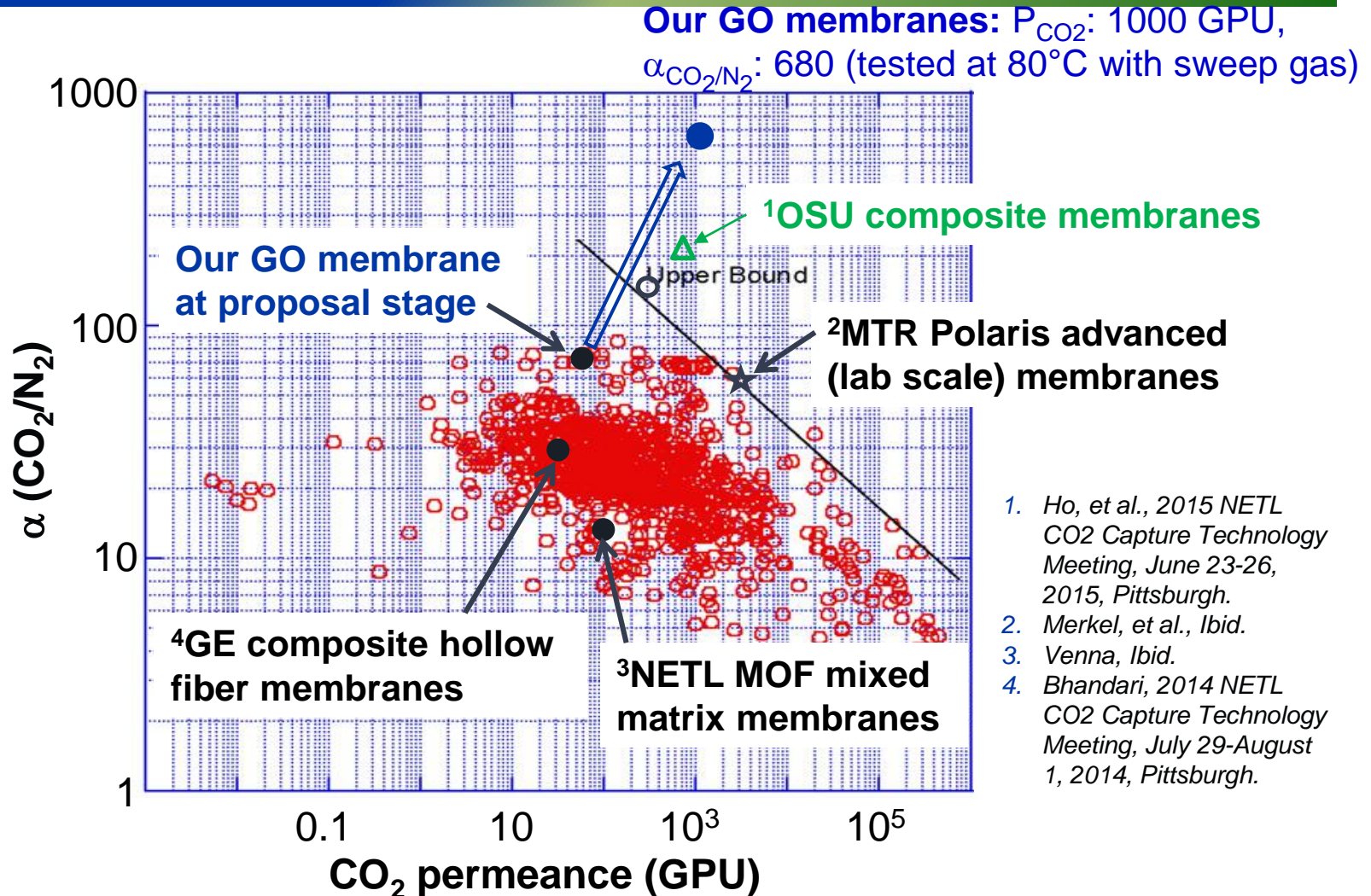


1. Ho, et al., 2015 NETL CO₂ Capture Technology Meeting, June 23-26, 2015, Pittsburgh.
2. Merkel, et al., *Ibid.*
3. Venna, *Ibid.*
4. Bhandari, 2014 NETL CO₂ Capture Technology Meeting, July 29-August 1, 2014, Pittsburgh.

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Future work overview/roadmap

GO Membrane Development

Task 6.0 (RPI) – Further GO optimization

Task 7.0 (GTI) – Performance stability testing of GO membranes using simulated flue gases

Task 9.1 (RPI) – GO membrane support for integrated testing

Integrated GO-PEEK Hybrid System

Task 8.0 (GTI) – Modification of an existing HFMC apparatus to GO-PEEK system

Task 10.0 (GTI) – CO₂ capture testing using integrated GO-PEEK hybrid system

Task 11.0 (Trimeric) – High-level techno-economic feasibility study

PEEK Membrane Development

Task 9.2 (ALaS) – PEEK membrane support for integrated testing

After the current project, steps can be taken to further reduce cost for GO-based membranes

- New process design
- Increase CO₂ permeance for GO membrane
- Advanced manufacture process to lower membrane costs

Hollow fiber configuration



← module
can be
used in
bench
scale

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- Increase CO₂ permeance for GO membrane
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Hollow fiber configuration



← module
can be
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scale

Flat sheet membranes to be used
in spiral wound configuration



Summary

- We are developing a transformational hybrid process for CO₂ capture combining a conventional gas membrane unit and a HFMC unit
- **The 3rd Generation PEEK fiber** developed to date
 - Fibers with intrinsic CO₂ permeance >3,000 GPU at 25°C
 - Membrane module effective in capturing CO₂ from low CO₂-concentration feeds with aMDEA solvent
- **GO membrane** developed to date
 - CO₂ permeance > 1,000 GPU and $\alpha_{\text{CO}_2/\text{N}_2} > 600$ obtained at 80°C for a humidified CO₂/N₂ mixture
 - Superior performance to GO-based membranes reported in the literature
- Future work will focused on further GO membrane development, integrated testing and TEA

Acknowledgements

- **Financial and technical support**



DE-FE0026383

- **DOE NETL José Figueroa and Lynn Brickett**
- **Dr. Yu Group**
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 - **Huynh Ngoc Tien**
 - **Jarvis Chen**
 - **Mahdi Fathizadeh**